

Attorney Docket No. 2002B132/2

AMENDMENTS TO THE SPECIFICATION**RECEIVED
CENTRAL FAX CENTER
SEP 15 2006**

Please replace paragraph [0001] with the following paragraph:

[0001] This application claims the benefit of Provisional Application No. 60/417,380 filed October 9, 2002, the disclosure of which are is incorporated by reference.

Please replace paragraph [0024] with the following paragraph:

[0024] In a specific embodiment, a slurry process may be carried out continuously in one or more loop reactors. The catalyst as a slurry or as a dry free flowing powder can be injected regularly to the reactor loop, which can itself be filled with circulating slurry of growing polymer particles in a diluent. Hydrogen, optionally, may be added as a molecular weight control. The reactor may be maintained at a pressure of from 27 bar to 45 bar, or preferably, from 36 bar to 43 bar and at a temperature in the range of from 38°C to 121°C, or preferably from 60°C to 105°C. Reaction heat can be removed through the loop wall since much of the reactor is in the form of a double-jacketed pipe. The slurry may exit the reactor at regular intervals or continuously to a heated low pressure flash vessel, rotary dryer and a nitrogen purge column in sequence for removal of the diluent and all unreacted monomer and comonomers. The ~~resulted~~ resulting hydrocarbon free powder can then be compounded for use in various applications. Alternatively, other types of slurry polymerization processes can be used.

Please replace paragraph [0028] with the following paragraph:

[0025] In addition, the conduit 400 preferably has a first monomer stream inlet 406. A first monomer stream 409 including propylene monomers can be introduced to the conduit 400 through the first monomer stream inlet 406 to provide a mixed catalyst stream (a mixture of catalyst and monomers) upon monomer contact with the catalyst, *e.g.*, when the catalyst is injected into the first monomer stream ~~418~~ 409. The monomer is preferably the same monomer as the monomer being polymerized in the polymerization vessel 404. For example, the monomer is preferably propylene. The mixed catalyst stream operates to increase the velocity of the catalyst entering the polymerization vessel 404. The first monomer stream inlet 406 may include a first conduit 407 having a first monomer valve 408. The first monomer valve 408 operates to

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provide a mixed catalyst stream having a velocity sufficient to prevent plugging of the conduit 400 during polymerization processes. The mixed catalyst stream velocity is dependent on individual system requirements, such as the conduit diameter.